Thermodynamic Functions of Adsorbed Molecules from Heats of Immersion¹

By George Jura and Terrell L. Hill

If N_s molecules are adsorbed on a solid of area α , it is of interest² to know the entropy and energy per molecule, $s_s = S_s/N_s$ and $E_s = E_s/N_s$, respectively. These functions can be calculated from two adsorption isotherms, measured at neighboring temperatures down to very low pressures, as illustrated in a paper by Hill, Emmett and Joyner.³ In favorable cases, with careful measurements, this can be an accurate method. On the other hand, in other cases very serious errors in the surface pressure, φ , and hence in s_s and E_s , may arise owing to uncertain extrapolation of the adsorption isotherm to p = 0. These errors can be especially serious in systems in which there are first order phase changes in the adsorbed phase: the phase change might be missed or the actual pressure at which it occurs may be uncertain.

An alternative and in general more precise method of obtaining s_s and e_s is to combine a computation of φ from a single adsorption isotherm with heats of immersion or ordinary integral calorimetric heats of adsorption, measured at the same temperature. Harkins and Jura⁴ used this method to obtain thermodynamic functions referred to the *solid surface*. We shall point out below the relations between the Harkins–Jura functions and the thermodynamic functions of the adsorbed molecules (*e.g.*, s_s and e_s). Incidentally, if the solid is perturbed by the adsorbed phase, the equations given below are still valid (see IX).

Let U_0 be the heat of immersion (in the liquid adsorbate) of the clean solid adsorbent, carried out in a container of fixed volume, and let U be the heat of immersion of the solid with N_s molecules adsorbed on it. Then it is easy to see that

$$\mathbf{E}_{\rm L}' - \mathbf{E}_{\rm s} = (U_0 - U)/N_{\rm s} \tag{1}$$

where E'_L is the internal energy of the liquid adsorbate per molecule (in equilibrium with vapor). Also,² using Eq. (1)

$$T(\mathbf{s}_{\mathbf{s}} - \mathbf{s}_{\mathbf{L}}') = [(U - U_{\mathbf{0}})/N_{\mathbf{s}}] + (\varphi/\Gamma) - kT \ln x \quad (2)$$
$$x = p/p_{\mathbf{0}}, \ \Gamma = N_{\mathbf{s}}/\Omega$$

assuming the vapor is a perfect gas and omitting a negligible volume term.

A comparison of the quantities calculated by Harkins and Jura⁴ in their Fig. 9 with the present notation gives the following relations between the two sets of functions

$$(\gamma_{\rm s} - \gamma_{\rm sf})_{\rm HJ} = \varphi \qquad (3)$$
$$(\epsilon_{\rm s} - \epsilon_{\rm sf})_{\rm HJ} = (U_0 - U)/\mathcal{R} = \Gamma(\mathbf{E}'_{\rm L} - \mathbf{E}_{\rm s}) \qquad (4)$$

(1) Presented at an American Chemical Society Meeting, New York, September, 1951.

(4) W. D. Harkins and G. Jura, ibid., 66, 919 (1944).

$$T(\mathbf{s}_{s} - \mathbf{s}_{sf})_{HJ} = \Gamma(\mathbf{E}'_{L} - \mathbf{e}_{s}) - \varphi = \Gamma[T(\mathbf{s}'_{L} - \mathbf{s}_{s}) - kT \ln x] \quad (5)$$

Whenever there is strong binding of the first layer to the surface, regardless of the details (solid adsorbents with small pores are excepted) and independent of any particular theory, one would expect a minimum in $s_s - s'_L$ at about the completion of a monolayer.⁵ This is because a virtually filled monolayer has fewer possible statistical configurations than either an incomplete monolayer or a complete monolayer plus an incomplete second layer. When combined with an estimate of the surface area per molecule in a filled monolayer, the above entropy minimum⁶ can be used as a method for surface area determination not dependent on a detailed theory. In the two cases worked out so far^{3,7} excellent agreement with the B.E.T. surface area is obtained. Minima in the function $(s_s - s_{sf})_{\rm HJ}$ do not have this simple theoretical relation to surface area, because of Γ and x in Eq. (5).

Alternatively, instead of using heats of immersion, E_s in Eq. (1) (relative to gas or liquid), for use in Eq. (2), may be found from integral calorimetric heats of adsorption,² as done by Drain and Morrison.⁷

Finally, we wish to examine the effects of errors in φ of the type mentioned above. For this purpose, we assume that errors in the heat measurements are negligible and that errors in φ arise only from pressures below the pressure region under discussion. Following V, let φ be the true spreading pressure, Φ the incorrect spreading pressure and a the error in Φ

$$\Phi(p,T) = \varphi(p,T) + a(T) \tag{6}$$

Let s_s be the correct entropy obtained from Eqs. (V-86, 93) and s'_s the incorrect entropy found by using Φ instead of φ in these equations. In this latter case, let a_1 be the value of a at T_1 and a_2 at T_2 . Then the error in the entropy is (V)

$$\mathbf{s}'_{\mathbf{s}} - \mathbf{s}_{\mathbf{s}} = \frac{1}{\Gamma} \frac{\Delta a}{\Delta T}$$
(7)
= $a_2 - a_{11} \Delta T = T_2 - T_1$

On the other hand, using Eq. (2) and an intermediate a and T, the corresponding error is $a / \Gamma T$. If ais of the same order of magnitude as Δa , the error in the heat calculation will thus be smaller in the ratio $\Delta T/T$. However, if the error is systematic (*i.e.*, $\Delta a \cong 0$), the opposite result is possible ($\Delta a / \Delta T < a/T$).

We have also

 Λa

$$\mathbf{E}'_{s} - \mathbf{E}_{s} = \frac{T}{\Gamma} \left(\frac{\Delta a}{\Delta T} - \frac{a}{T} \right) \tag{8}$$

which corresponds to Equation (7).

DEPARTMENT OF CHEMISTRY AND CHEMICAL ENGINEERING UNIVERSITY OF CALIFORNIA

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⁽²⁾ T. L. Hill, J. Chem. Phys., **17**, 520 (1949), hereafter referred to as V; *ibid.*, **18**, 246 (1950), hereafter referred to as IX; Trans. Faraday Soc., **47**, 376 (1951) (in this paper H^{σ} should be replaced by \mathcal{H}^{σ} in lines 29, 31, 33 and 34, p. 378).

⁽³⁾ T. L. Hill, P. H. Emmett and L. G. Joyner, THIS JOURNAL, **73**, 5102 (1951). Errata: Change s_8 to \bar{s}_8 in Eq. (1), in third line below Eq. (2), third equation, in third line below Eq. (17), and in line 17 of "Results and Discussion." Change H_8 to \bar{H}_8 in line below Eq. (6), and in Eq. (7). See THIS JOURNAL **73**, 5933 (1951).

⁽⁵⁾ See, for example, T. L. Hill, J. Chem. Phys., 17, 772 (1949).

⁽⁶⁾ In many cases the differential entropy curve will be available but not the molar integral entropy curve. In this case, if there is a "loop" in the differential entropy ^{2,8,7} the surface area can be estimated by assuming that a monolayer is completed at the inflection point in the loop.
(7) L. E. Drain and J. A. Morrison, American Chemical Society Meeting, New York, September, 1951.